

Study on the Green Ammonia Supply Chain: Production, Storage and Export of Green Ammonia from India via seaborne transport

Knowledge Dissemination Workshop



- 1. Project Scope and Approach**
- 2. Key findings on techno-economic assessment**
- 3. Key Findings from Export Infrastructure Study**



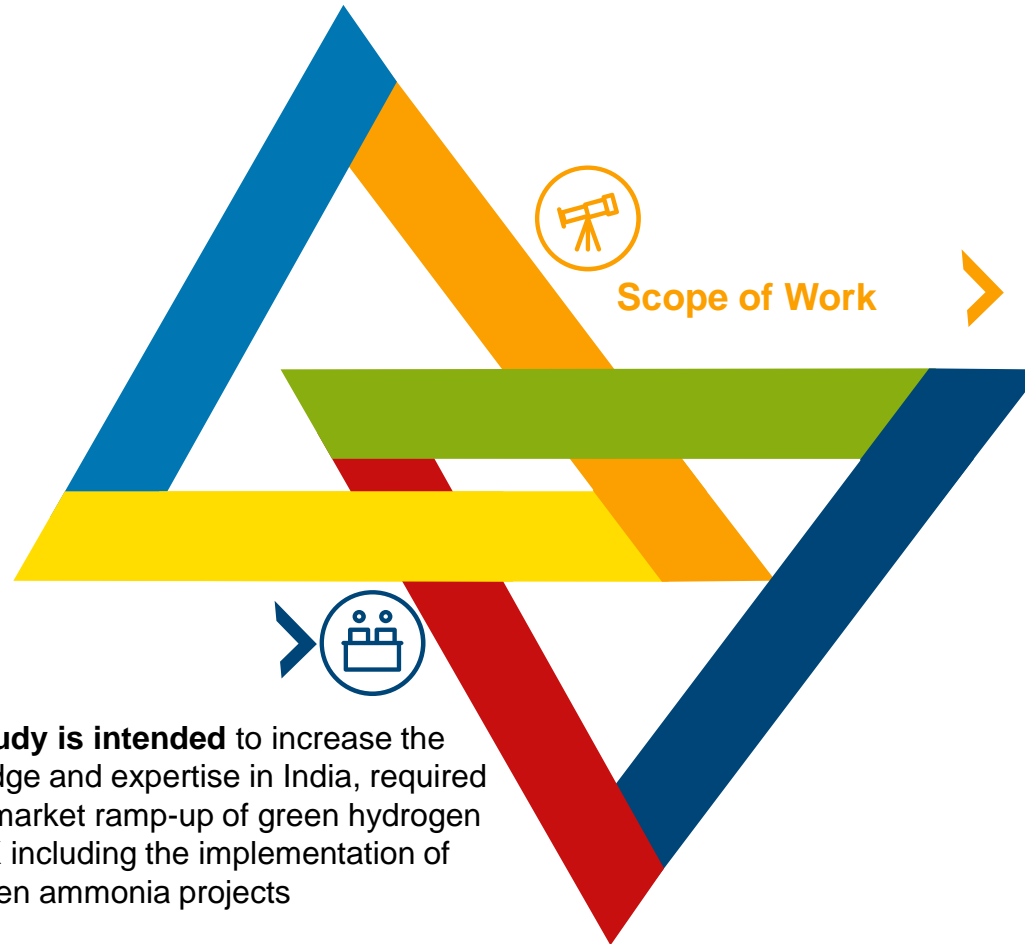
Project Scope and Approach

Context: Green ammonia demand from EU offers export opportunity from India

- EU is likely to import more than **10 MTPA GH₂** by 2030
- With the evolving directives, such as **RED, REFuelEU**, demand will increase further

- India's **low-cost renewable** could help the country in emerging as an export hub
- Significant **in-house demand** and **Government initiatives** will drive development of eco-system
- **~20 MTPA GNH₃** capacity is already announced and MoUs have been signed

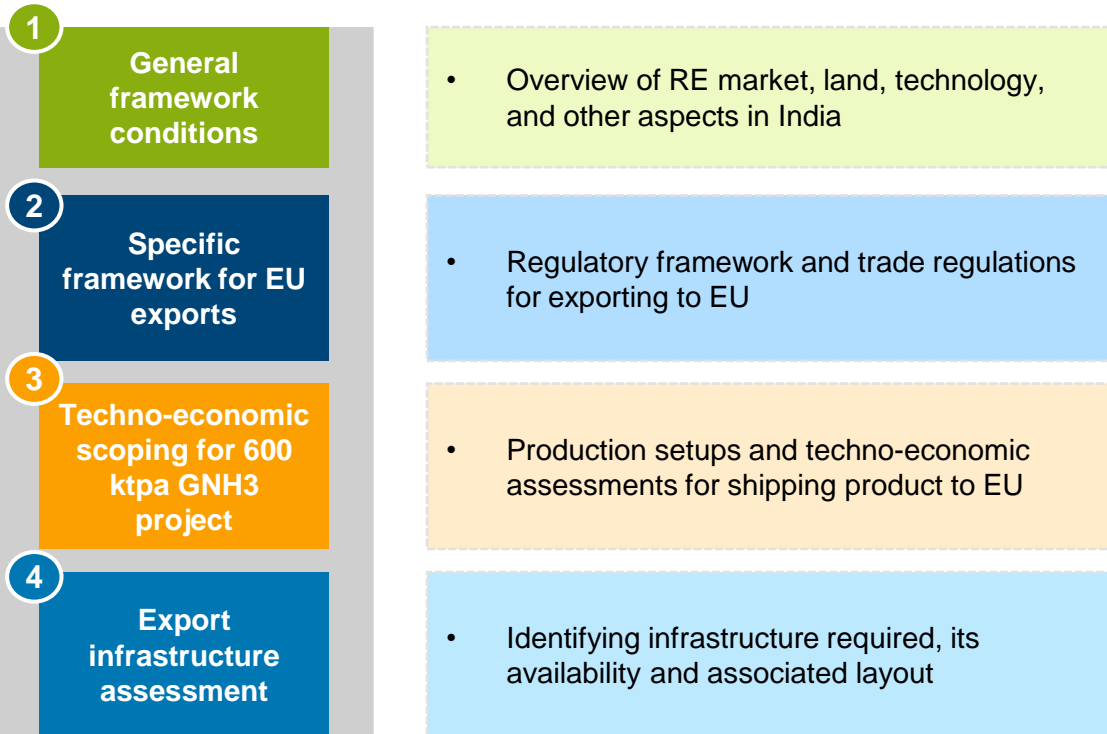
Context: A techno-economic assessment of production, storage and export of GNH3 from India is required to assess the feasibility



- **Review of RE market in India** pertaining to GNH3 production
- Overview on **land, water and infrastructure, local technology availability and sustainability dimensions along value chain**
- **Review of regulatory framework, certification scheme, trade regulations** in India and EU/Germany
- **Techno-economic scoping** for 600 kTPA green ammonia production facility
- Assessment of **export infrastructure, safety requirements** for seaborne transport

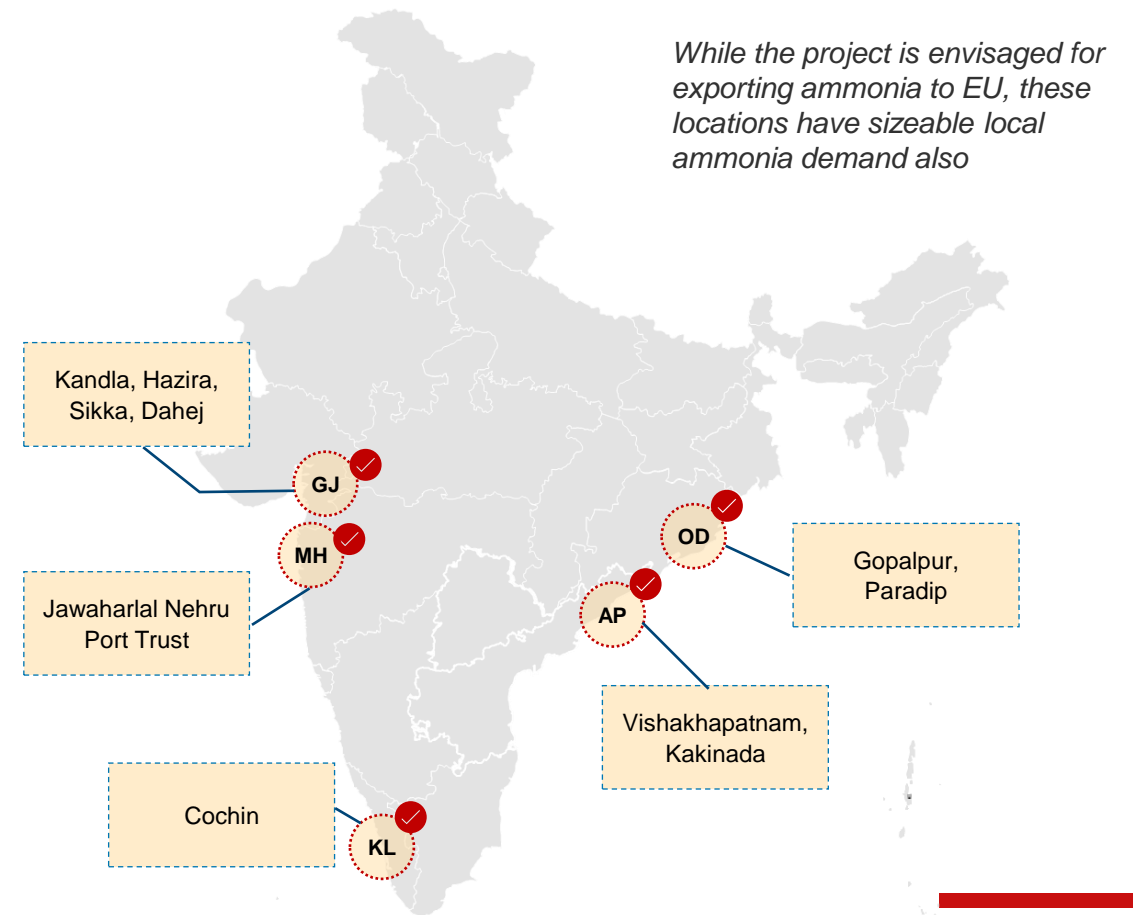
A modular approach was undertaken to assess the 5 potential states for ammonia exports to Europe

Step by step approach to assess feasibility of exports



Assessment of the landed cost of ammonia in European ports

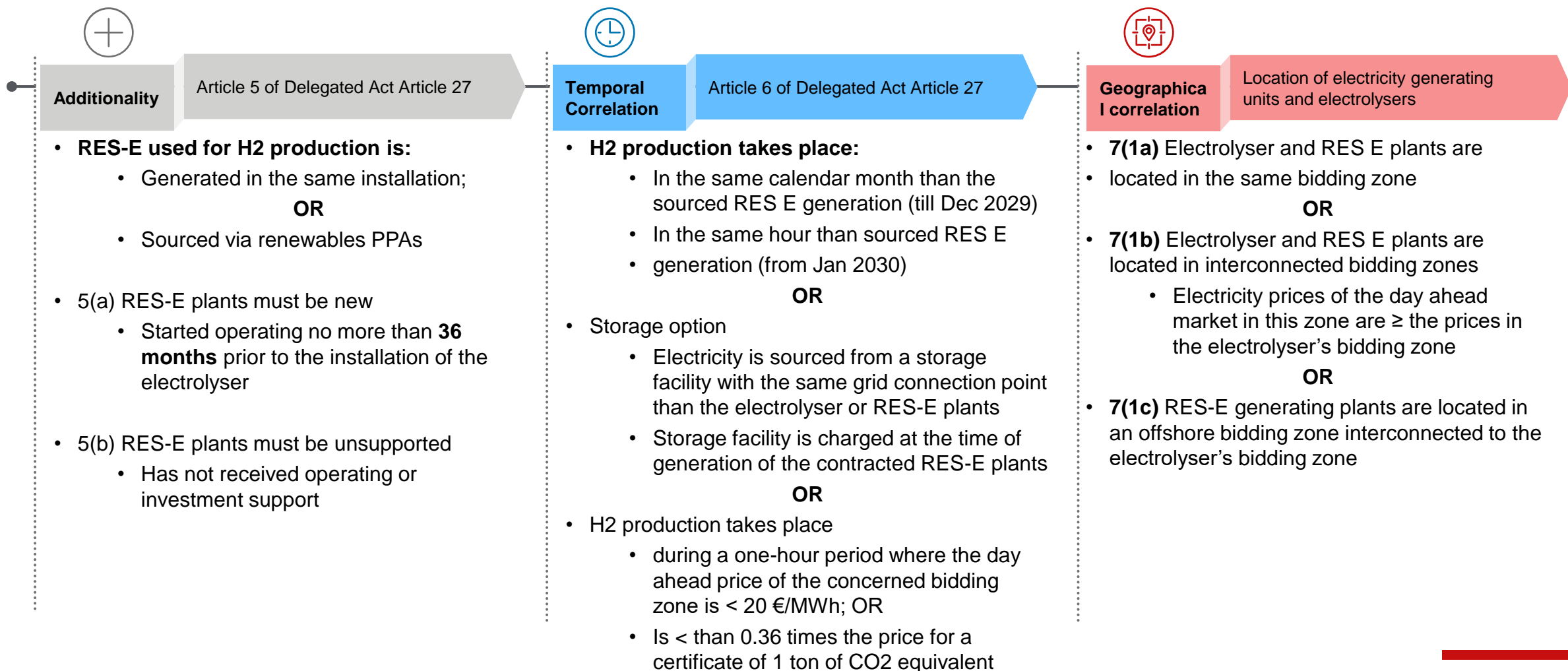
5 coastal states have been shortlisted for assessment



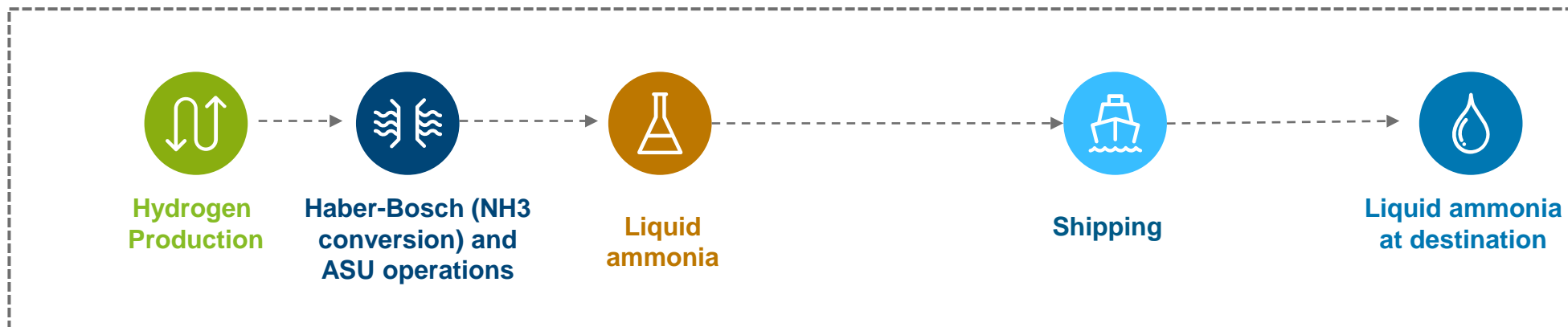


General and Specific Framework Conditions

RED-II and 1st set of Delegated Acts have specified criteria for labelling green hydrogen and ammonia



As per RED-II and 2nd set of Delegated Acts, GNH3 having emission intensity up to 0.61 tCO₂eq./t can be exported to EU



GHG threshold requirement for Green Ammonia
~**0.61 tCO₂e/t**



Energy Use	Renewable electricity/ GRID/ GDAM Electricity consumption: 56 kWh/kg H₂ production, 6 kWh/kg for compression, 0.3 kWh/kg NH₃ production (includes Haber-Bosch and ASU operations)	MGO used during shipping 16 MT/day during shipping; 9 MT/day during port call, anchorage Boil off-rate of ammonia: 0.04% per day Reliquification: 0.224 kWh/kg Pumping: 0.25 kWh/m³ NH₃ (at both source and destination)
Emission Intensity	0 tCO₂e/t for RE power; State grid intensity for Grid power and NIL for GDAM	3.15 tCO₂/t emissions from MGO combustion 0.711 tCO₂eq./MWh for Indian Grid 0.59 tCO₂eq./MWh for EU/German Grid

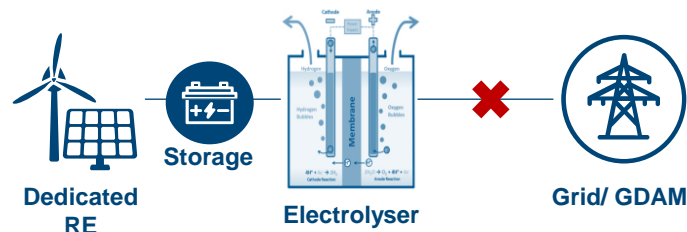
Margin available
for use of fossil fuel
~**0.51 – 0.55 tCO₂e/t NH₃**



Permissible grid power could be in range of 7.8 – 8.0%

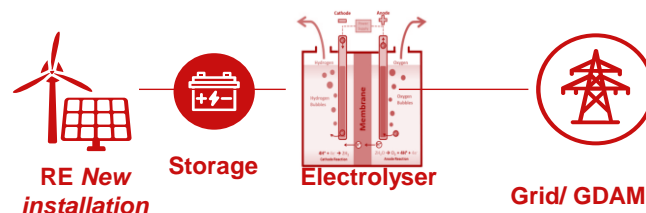
Three production setups have been assessed for GNH3 production and export to EU

Option 1: Electricity produced off-grid



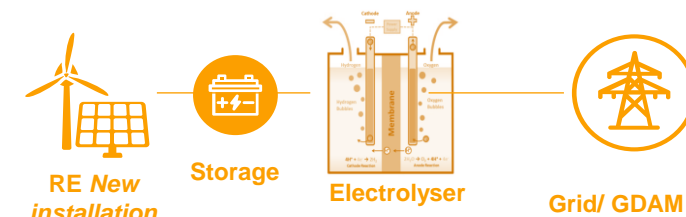
- 100% RE based electrolyser and ammonia loop operations
- Lowest emission intensity among all options for green ammonia production
- RE and BESS setup is considered to be captive

Option 2: Co-located RE + BESS + Permissible Grid + GDAM



- Permissible Grid electricity (as per emission thresholds and state emission intensity), RE+BESS and GDAM (Green Day Ahead Market) are utilized for the electrolyser and ammonia operations.

Option 3: Co-located RE + BESS + Optimized Grid + GDAM

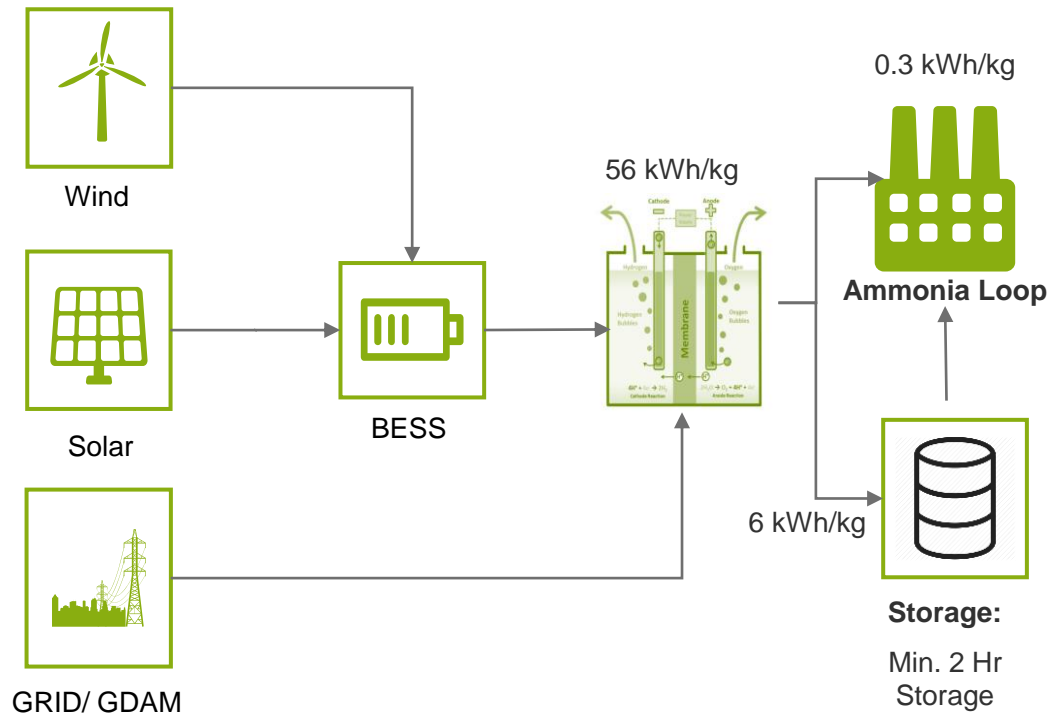


- Optimized Grid electricity (basis optimization of annual fixed cost) and RE+BESS and GDAM (Green Day Ahead Market) are utilized for the electrolyser and ammonia operations.

Respective regional solar and wind generation profiles of the 5 target states have been considered for optimizing RE, BESS and storage sizing

Approach: The sizing of each production setup has been determined using an Excel based optimization tool

System Configuration



The ammonia loop is run constantly throughout the day basis which the sizing of RE, Electrolyser, BESS, and Storage are optimized

Objective function and key assumptions/constraints

- The objective function targets to minimize the annual expenditure of the electrolyser, storage, RE and BESS setup.
- $AFC = f(\text{Solar}, \text{Wind}, \text{BESS}, \text{Electrolyser}, \text{Storage})$
- $Opex = f(\text{Electricity from grid}, \text{Electricity from GDAM})$
- Objective function** = $\text{Min} (AFC + Opex)$
- Maximum Grid offtake** ~7 – 8% % based on EU import criteria
- Minimum load of electrolyser – 30%

Particular	Unit	AFC value	Capex
Annualized solar capex	INR Cr/MW	0.59	INR 4.5 Cr/MW
Annualized Wind capex	INR Cr/MW	0.88	INR 7.5 Cr/MW
Annualized 2hr BESS capex	INR Cr/MW	0.58	INR 3.5 Cr/MW
Annualized Alkaline electrolyser capex	INR Cr/MW	0.9	USD 600k/MW
Annualized storage capex	INR Cr/tonne	2	USD 1 Mn/ton
Landed cost from GDAM	INR/kWh	~8 – 9	-

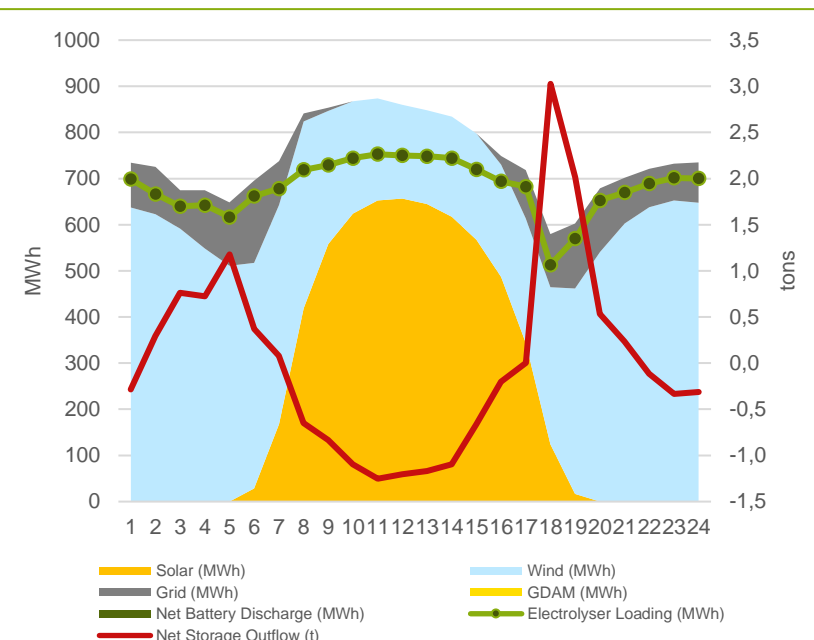
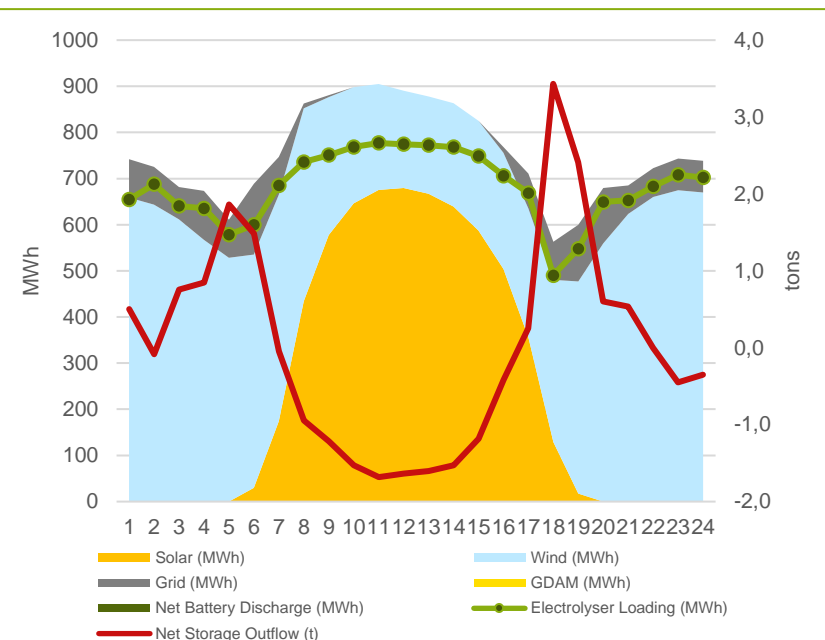
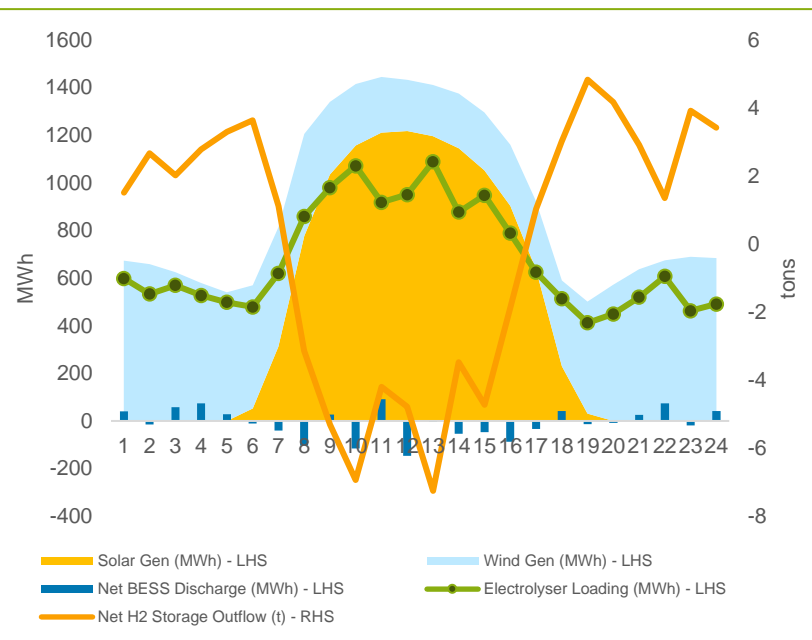
Sample output of optimization modelling (for Gujarat location)

GJ solar and wind profile

Particular	Unit	Offgrid (RE+BESS)	RE+BESS+7.8% Grid	RE+BESS+GRID
GRID Power	%	0%	7.8%	10 – 12%
Electrolyser Capacity	<i>MW</i>	1050 - 1150	750 - 900	730 - 800
Solar	<i>MW</i>	1400 - 1600	800 - 1000	800 - 900
Wind	<i>MW</i>	1500 - 1700	1400 - 1600	1450 - 1550
H2 Storage Capacity (GH2)	<i>Tonnes</i>	70 - 90	20 - 30	20 - 30
Electrolyser CUF	%	60 – 70%	80 – 90%	85 – 90%
BESS (2 hr)	<i>MW</i>	400 - 500	0	0.0
Landed Cost of electricity	<i>INR/kWh</i>	3.8 – 4.5	3.30 – 4.00	3.30 – 4.00
LCOA	<i>USD/ton</i>	900 - 1050	900 - 1000	850 - 1000

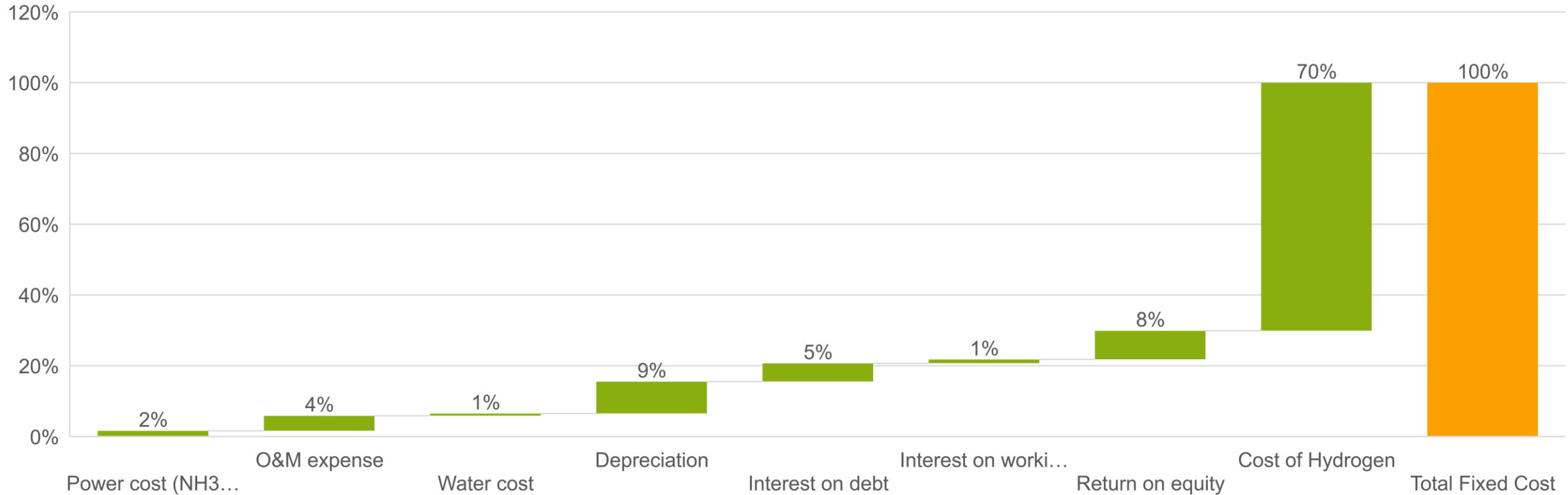
Sample output of optimization modelling (for Gujarat location)

System loading



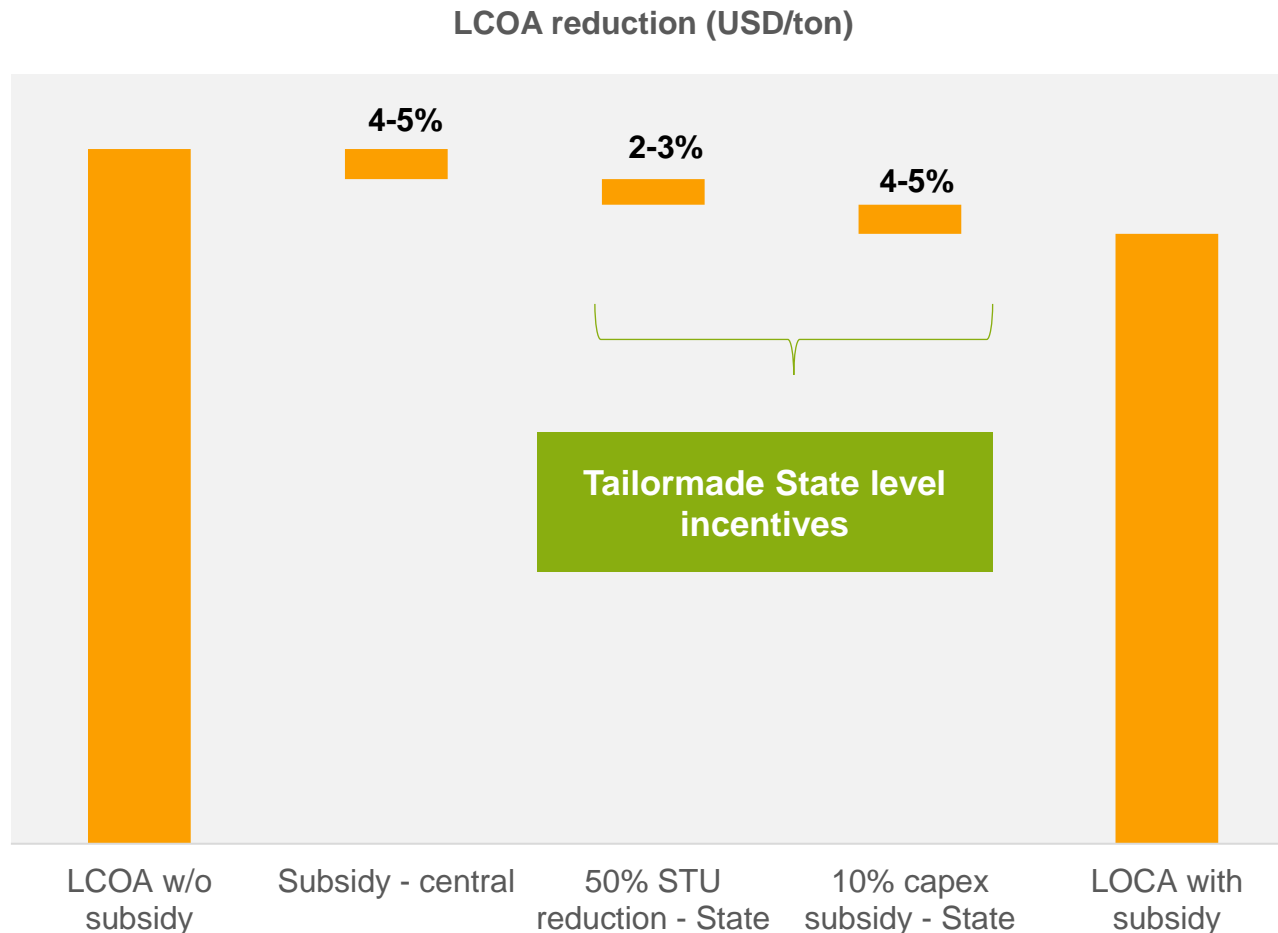
Ammonia cost breakdown

Under Option 2: Co-located RE + BESS + Permissible Grid and GDAM procurement



Reduction in LCOH is critical to bridge the LCOA gap between grey and green ammonia

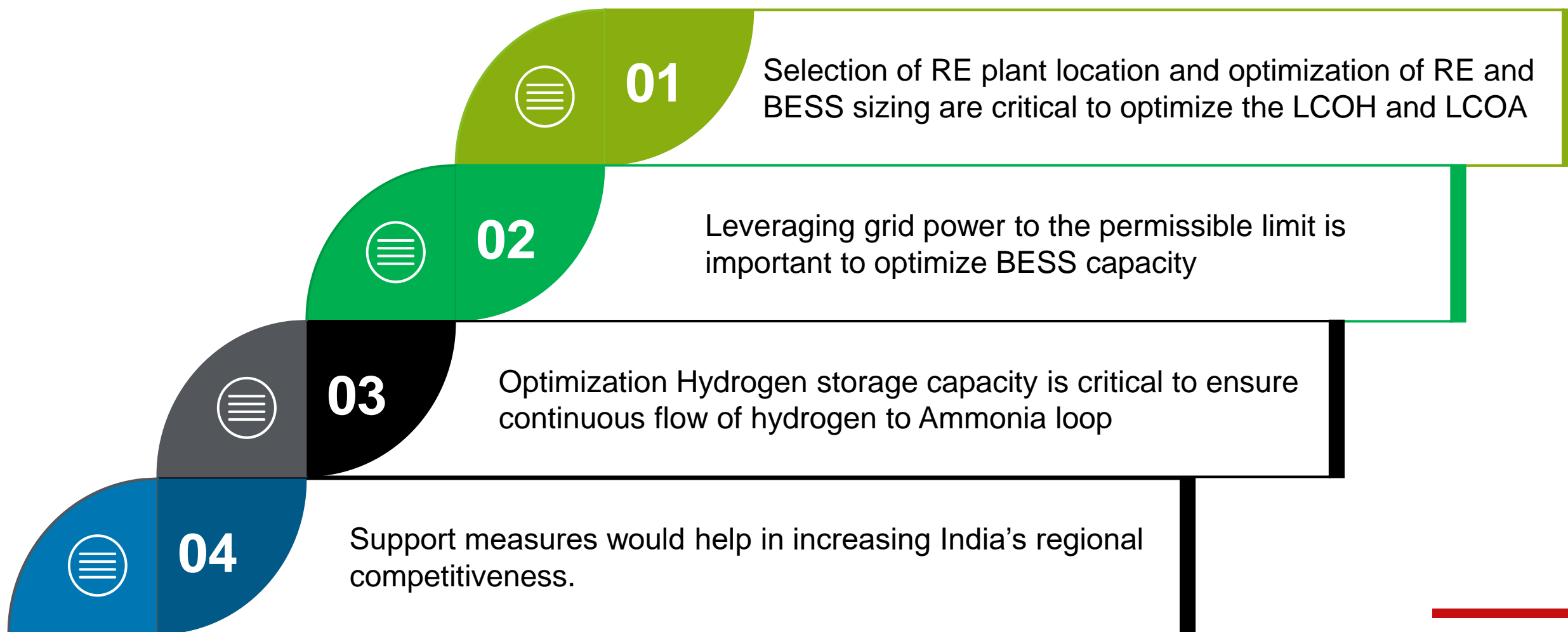
Impact of subsidies on Green Ammonia – Cost of production can be reduced by 10 – 12% through central and state level subsidies



Gross Impact on LCOA

- Average subsidy of **INR 30/kg** can reduce the **LCOA by 2-3%**
- Electrolyzer PLI can reduce the **LCOA by 1-2%**
- STU charge waiver and Capex subsidy can further reduce **LCOA by 6-8%**

Key findings from techno-economic assessment





Export Infrastructure Study

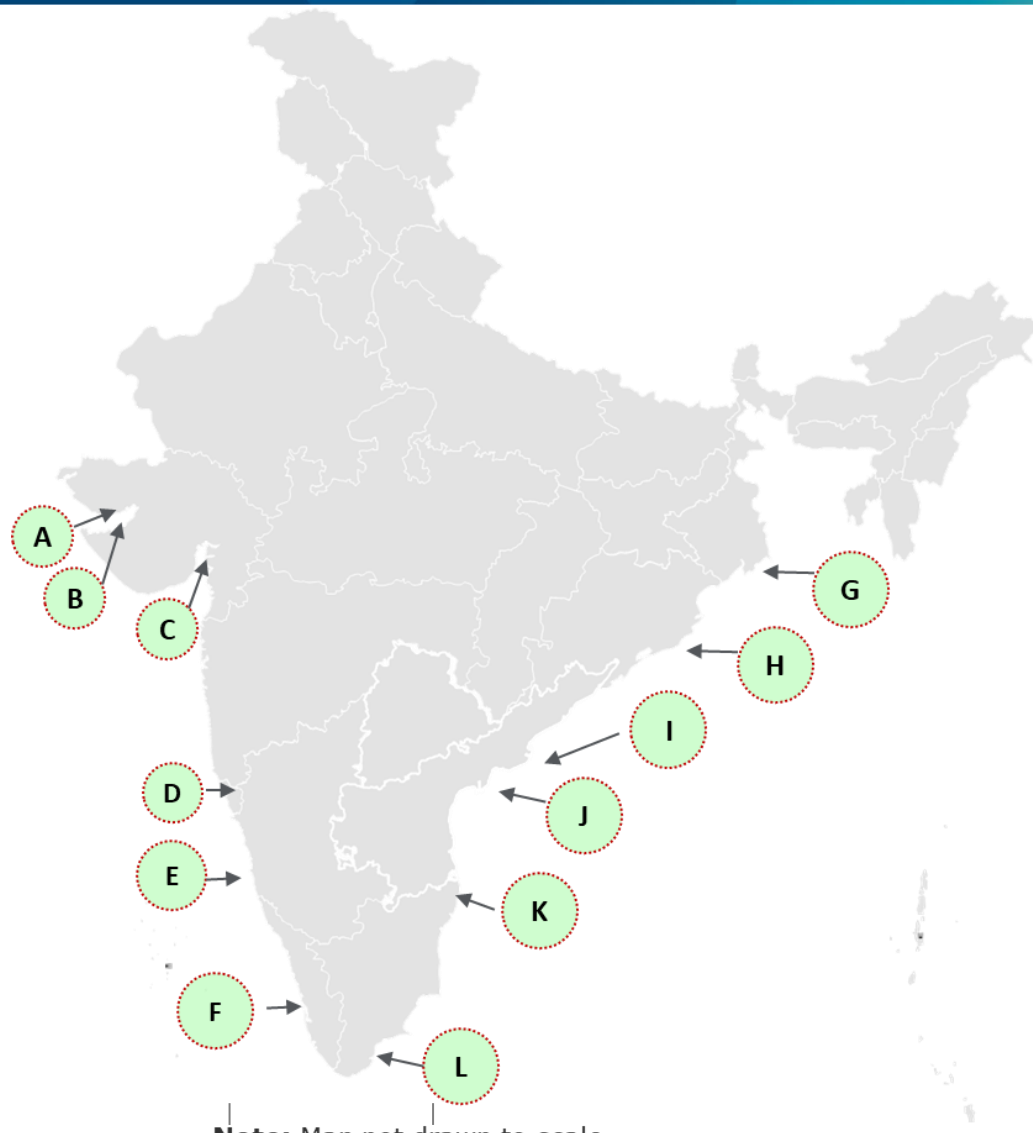
Options for seaborne transport of green ammonia from India to Europe

1. Gas carriers with onboard refrigeration system offer an economical and proven mode of shipping ammonia.
2. For long distance ocean shipments of ammonia; Large Gas Carriers and Mid Size Gas Carriers with refrigerated cargo tanks are used. Very Large Gas Carriers are not currently being used for ammonia shipments.

View on vessels availability for globally shipping ammonia

- 114 unique vessels (with a cumulative 2.5 Million DWT) were deployed for shipping ammonia over last 2 years
- Cumulative ammonia carrying capacity of the unique vessels deployed in CY 2023 and in CY 2022 add to 1.9 MMT
- 200 LPG tankers in operation with typical storage capacity of $\geq 40,000$ MT are cable of carrying ammonia at full refrigeration
- 20 Large Gas Carriers and 140 Mid Size Gas Carriers in service
- 1,200 LPG tankers could also become suitable for carrying ammonia shipments
- Existing fleet of more than 600 LNG vessels could also handle ammonia post retrofitting
- 19 Very Large Ammonia Carriers new building ships orderbook of 88,000/93,000 CBM each with deliveries commencing from 2026 onwards.

Summary of Export infrastructure



Note: Map not drawn to scale

List of seaports handling ammonia imports in bulk

West Coast India

A	Kandla
B	Sikka
C	Dahej
D	Mormugao
E	Mangalore
F	Cochin

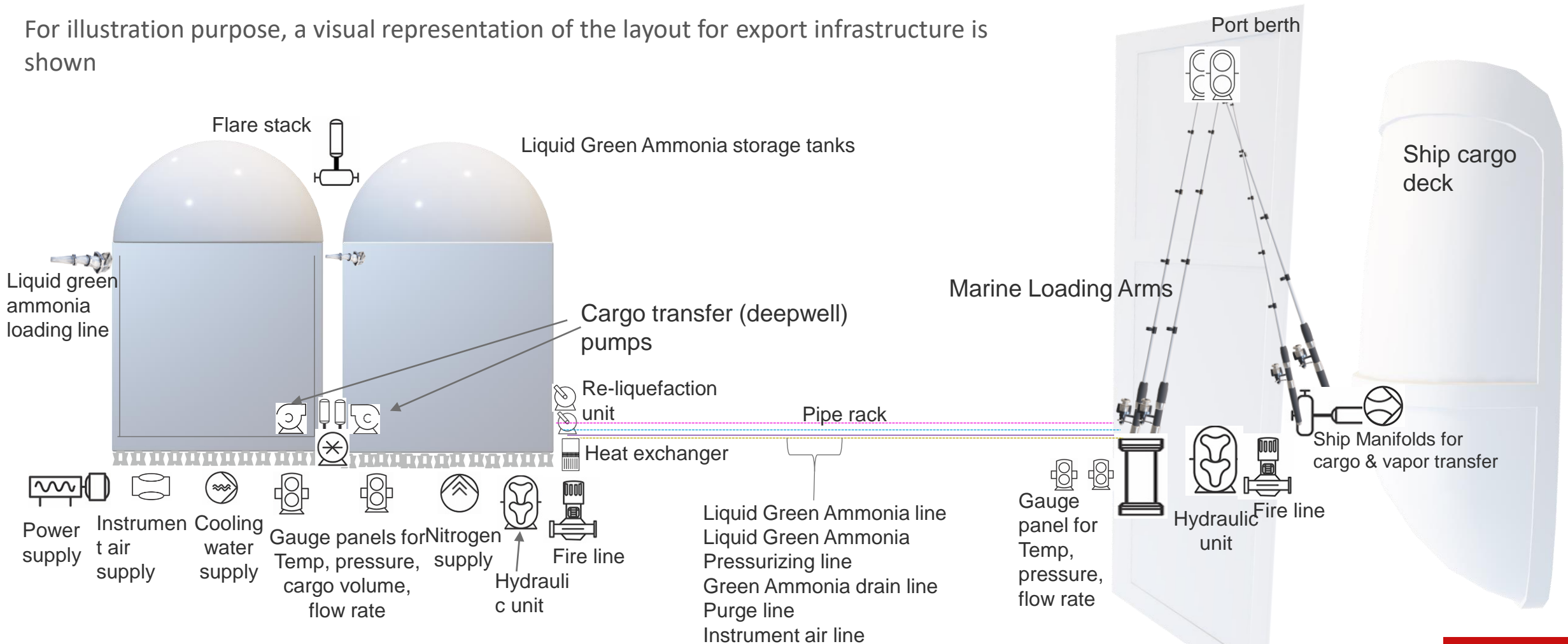
East Coast India

G	Haldia
H	Paradip
I	Visakhapatnam
J	Kakinada
K	Ennore
L	Tuticorin

Export terminal may comprise of Marine Loading Arms with related cargo transfer marine infrastructure including a dedicated pipe rack at an existing port berth. Storage tanks at port premises may not be mandatorily established. Direct transfer of green ammonia from storage tanks set up at the production facility to vessels may likely be a more viable proposition.

Layout of Export infrastructure

For illustration purpose, a visual representation of the layout for export infrastructure is shown



Note: Layout not drawn to scale

Green Shipping: Investigation on multipurpose use of ammonia terminal for fueling of ammonia powered ships

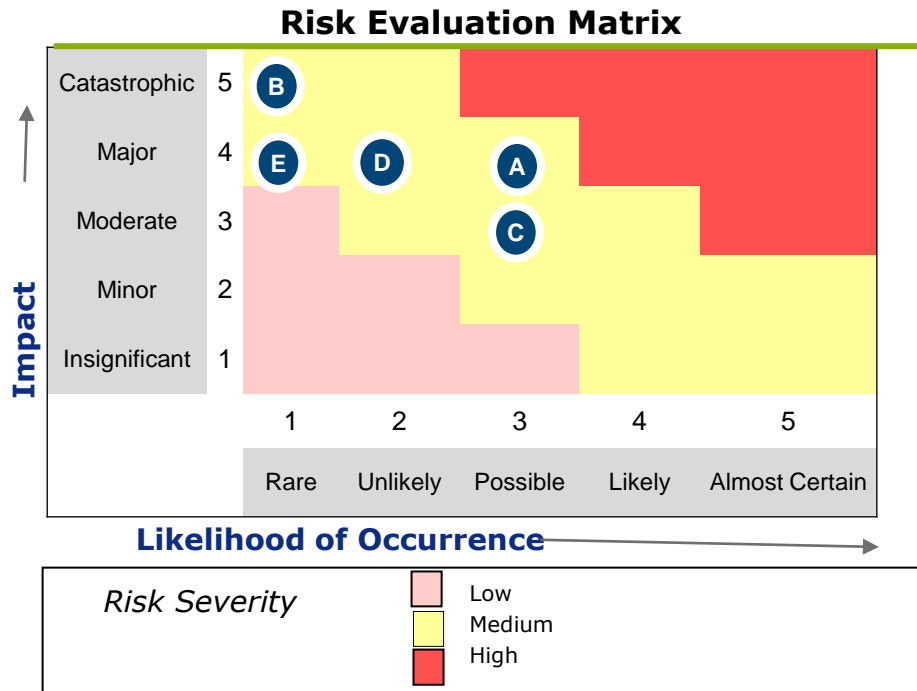
Bunkering options

- Green Ammonia as bunker is supplied using marine loading arms at terminal for ships brought alongside
- Green ammonia is filled in bunker supply vessels for bunkering ammonia powered ships located at alternate berths/offshore locations. Green ammonia is filled in bunker supply vessels from marine loading arms.

	Scenario 1	Scenario 2	Scenario 3	Scenario 4
Bunkering vessel	Pressurized tanks	Semi-refrigerated tanks	Pressurized tanks	Semi-refrigerated tanks
Ship to be bunkered	Pressurized tanks	Pressurized tanks	Semi-refrigerated tanks	Semi-refrigerated tanks
Green ammonia transfer arrangements	Bunkering vessel transfers green ammonia using general transfer pumps. Vapor return system from ship taking bunkers to the bunkering vessel will be needed.	Bunkering vessel transfers green ammonia using installed heater (sea water heated system) and booster pump. Vapor return system from ship taking bunkers to the bunkering vessel will be needed. Re-liquefaction system on bunkering vessel is needed to handle high pressure vapor return.	Bunkering vessel will need liquefaction plant to reduce pressure by lowering temperature. Vapor return system from ship taking bunkers to the bunkering vessel will be needed. Compressor on bunkering vessel is needed to increase pressure of vapor return.	Bunkering vessel may need cooling arrangement. Vapor return system from ship taking bunkers to the bunkering vessel will be needed.

Sources: Assessments from IACS member firms

Analysis of safety aspects for exporting green ammonia via seaborne transport



A

Risk: Non-compliance to safety protocols during ship loading and unloading, cargo changeover (i.e. changing from LPG to ammonia)
Mitigation: Regular training of seafarers wrt SOPs for cargo operations, flushing and draining systems, etc.

B

Risk: Severe collision or stranding that could lead to cargo tank damage and uncontrolled release of ammonia
Mitigation: Compliance to traffic separation schemes be ensured, spill containment systems to be placed on board the vessels, remote stations for monitoring, etc.

C

Risk: Operating personnel come in contact with ammonia vapors
Mitigation: Operating personnel to adopt safe working practices and ensure wearing Personal Protective Equipments (PPE). Functional emergency showers and eyewash

D

Risk: Breach in ammonia tank and associated piping
Mitigation: Dry drip tray (with a drain leading to enclosed tank), foam/dry chemical powder spill mitigation system to be placed onboard, etc.

E

Risk: Cargo comes in contact with parts containing Cu, Zn or alloys
Mitigation: Compliance to IGC Code for ships structural aspects to be ensued, Ammonia test for stress corrosion resistance as per ISO 6957:1988/IACS

Compliance to the Rules and Regulations as per the IGC Code, OCIMF, SIGTTO Guidelines, ISGOTT, IACS , etc.
 is mandated for safely exporting green ammonia via seaborne transport.

Sources: The International Code of the Construction and Equipment of Ships Carrying Liquefied Gases in Bulk (IGC Code), Oil Companies International Maritime Forum (OCIMF), Society of International Gas Tanker and Terminal Operators (SIGTTO), International Safety Guide for Oil Tankers and Terminals (ISGOTT), International Association of Classification Societies (IACS)

Questions?



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We will be sharing the presentation with the webinar participants

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The International Hydrogen Ramp-up Programme (H2Uppp) of the German Federal Ministry for Economic Affairs and Climate Action (BMWK) promotes projects and market development for green hydrogen in selected developing and emerging countries as part of the National Hydrogen Strategy.